

# Experimental analysis of heat transfer enhancement within tube in tube heat exchanger by using nano fluid and jagged twisted tape inserts

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## Abstract

Heat transfer & friction factor characteristics of CuO/water nanofluid have been experimentally inspected within tube in tube counter flow heat exchanger. The CuO/water nanofluid with nanoparticle 0.1% by volume was engaged in circular tube equipped with full-length square jagged copper twisted tape inserts as a turbulators. Square jagged twisted tape inserts having twist ratios 4, 6 and 7 were used alternately by keeping the 0.1 vol% constant concentration of nano particles. The experimentation were performed and different readings for different set were recorded in turbulent regime with Reynolds number in between 2700 and 54000, to assessment of heat transfer increment and the friction factor. The attained results release that Nusselt number intensifies with increase in Reynolds number and shrinkage in twist ratio of twisted tape inserts. The synchronized use of square jagged twisted tape insert with twist ratio 4 and CuO/water nanofluid gives significant increase in Nusselt number value than that of the plain tube in tube heat exchanger.

**Keywords :** Heat transfer enhancement, Nanofluids, Tube in tube heat exchanger, Square jagged twisted tape inserts, Twist ratio.

## 1. Introduction

A variety of strategies has been used to decrease the size of the heat exchanger, running costs and to increase heat transfer rate. In different fields for excellent heat transfer performance, nanofluids are used as heat transfer medium. Most of the investigators measured thermal conductivity [1-3], as well as developed some imperial relations for thermal conductivity [4-7]. The literature delivers a more thorough analysis of the study on the preparation processes and thermal property parameters of nanofluids [8]. Additionally, a selection criteria for nanofluids has been researched for use in practical applications of nanofluids [9]. Free convection and forced convection are two essential heat transfer techniques in the world of heat exchange equipment. Numerous studies on free convection have been documented in the literature. Shi et al. [10] used experimental and numerical modelling techniques to conduct research on the free convection of  $\text{Fe}_3\text{O}_4@\text{CNT}$  nanofluids in a rectangular cavity under magnetic field conditions. The results showed that the magnetic field's direction can control how well nanofluids conduct heat. Selimefendigil et al. reports [11, 12], the free convection of CNT/water nanofluids in a two-dimensional enclosure with a corrugated partition and three different types of nanofluids in a three-dimensional cavity with rotating circular cylinders were both studied using numerical methods. It was found that the rotational direction of circular cylinders also significantly affects heat transfer, and that the thermal performance of nanofluids diminishes with the height of the triangle waves in the two-dimensional enclosure. A numerical simulation research on the free convection of MWCNT- $\text{Fe}_3\text{O}_4$ /water nanofluids in a square cavity full of porous media was given by Sajjadi et al. [13]. Results indicated that the thermal performance can be improved by raising the Darcy number and porosity. Numerous studies have been done on the natural convection of nanofluids in different cavities.

The application of CuO nanofluids within a tube in tube heat exchanger with twisted tape is the attention of the current effort. A set of square jagged twisted tape inserts ( $y/w = 4, 6, \text{ and } 7$ ) were used with only one concentration of nano particles as 0.1% by volume, and Reynolds numbers between 2700 and 54,000.

## 2. Experimentation

### 2.1. Nanoparticles concentration calculation & Nanofluid preparation

CuO nanoparticles with an average size of  $<80$  nm and a density of  $6349 \text{ kg/m}^3$  are purchased from Intelligent Materials Pvt. Ltd., which works in association with Nanoshel LLC, a corporation with its headquarters in the United States.



**Figure-1:** Photograph of CuO nanoparticles

The law of mixture formula is used to determine how much CuO nanoparticles are needed to prepare nanofluids. The CuO nanoparticles are extremely precisely weighed using a sensitive scale with a 0.1 mg resolution. The following relation is used to determine the weight of the nanoparticles needed to prepare 100 ml of CuO nanofluid at a specific volume concentration using distilled water as the base fluid:

$$\% \text{ volume concentration} = \frac{\left[ \frac{W_{CuO}}{\rho_{CuO}} \right]}{\left[ \frac{W_{CuO}}{\rho_{CuO}} + \frac{W_{bf}}{\rho_{bf}} \right]}$$

Table-1 Volume concentrations of CuO nanoparticle with corresponding weight

Sr. No.	Volume concentration (φ) (%)	Weight of nanoparticles (W <sub>CuO</sub> ) (Grams)
1	0.1	0.60872
2	0.2	1.21865

Nanofluids can be prepared using either by a one-step method or by a two-step method. A two-step approach is used to create a CuO/Distilled water-based nanofluid with a volume concentration of 0.1%. Nanoparticles are mixed with distilled water during processing. For an hour, a magnetic stirrer is utilised in the homogenise mixer to dissolve accumulations.



**Figure-2:** Sample CuO/water nanofluid

**2.2. Experimental apparatus**

The tube in tube heat exchanger experimental setup is represented in Figure 3 and 5, respectively, along with its schematic layout and actual experimental setup. The experimental setup consists of a test section having inner tube of copper having inside diameter 19.8 mm and outer diameter of inner tube is 25.4 mm. Outer tube is of stainless steel having inner diameter 32 mm and outer diameter is 38 mm. In order to minimise heat losses to the atmosphere, the exterior pipe is effectively insulated with 15mm thick asbestos rope. Cold water and hot nanofluid flow rates are measured using two rotameters, each with a flow range of 100-1000 LPH. Two centrifugal pumps of ½ HP of capacity 2000 LPH are used. Four flow control valves are used. and collection tanks are used. For the purpose of measuring the pressure drop, two pressure tapings—one at the test section's inlet and the other at its outlet are offered and connected by pipes to the inverted U-tube manometer. Through a multipoint digital temperature indicator, four-temperature sensors (RTD) PT-100 3-wire are utilised to detect the intake & exit temperatures of hot nanofluid and cold water (i.e., Th1, Th2, Tc1, and Tc2). A hot nanofluid tank is equipped with 1500-watt electric heater. CuO-water nanofluid and different twisted tape inserts are used.



Figure-3: Experimental set up

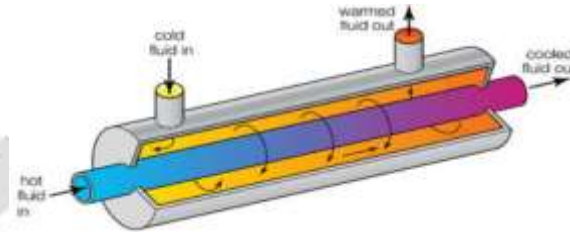


Figure-4: Cut section model of test section

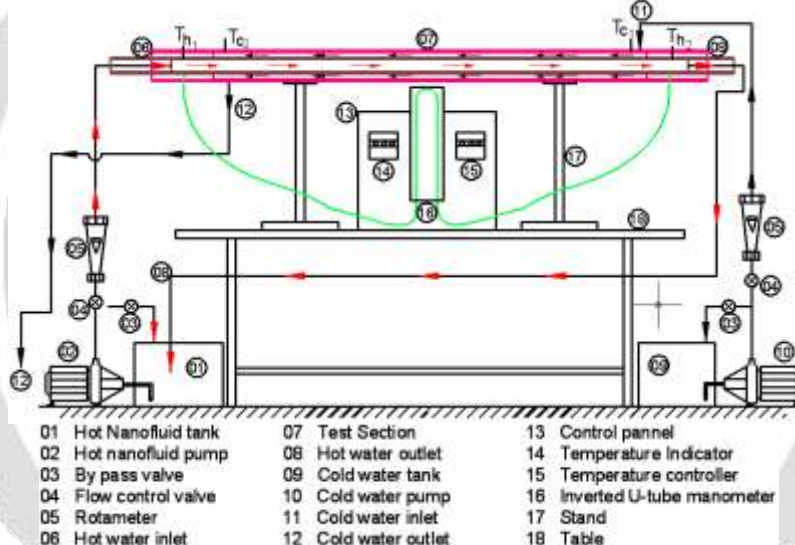


Figure-5: Schematic of experimental set up

2.3. Experimental Process

Place the nanofluids in the hot nanofluid tank, and set the temperature to the desired value i.e. 70<sup>0</sup>C. Open every valve, flow metre, and pump in the experimental system, start the two loops of working fluids, and thoroughly inspect the experimental system for leaks. Open transmitters of U-tube differential manometer. For different hot water flow rates, such as 300, 400, 500, 600, 700, 800, and 900 LPH, note all the readings. Repeat the same process for all sets (i.e. plane tube with base fluid, nanofluid with different sets of twisted tape inserts, shown in the figure-5, 6, and 7). After completion of testing, turn off the pumps, the water heater, and the thermometer. Finally turn off the main power.



Figure-6: Square jagged copper twisted tape insert (twist ratio, y/w=7)



**Figure-7:** Square jagged copper twisted tape insert (twist ratio,  $y/w=6$ )



**Figure-8:** Square jagged copper twisted tape insert (twist ratio,  $y/w=4$ )

### 3. Experimental data processing

#### 3.1. Water Properties

i) Mean bulk temperature of nanofluid hot water

$$T_{bh} = \frac{Th_2 + Th_1}{2}$$

ii) Properties of cold water

$$T_{bc} = \frac{Tc_2 + Tc_1}{2}$$

#### 3.2. Heat given by hot nanofluid

$$Q_h = [m C_p (T_{h1} - T_{h2})]_h$$

#### 3.3. Heat given by cold water

$$Q_c = [m C_p (T_{c2} - T_{c1})]_c$$

#### 3.4. Average heat transfer

$$Q_{avg.} = \frac{Q_c + Q_h}{2}$$

#### 3.5. Heat transfer coefficient (Overall)

$$Q_{average.} = A_s \Delta T_m U$$

i) Heat transfer surface area of tube

$$A_s = L \pi d_i$$

ii) LMTD (Logarithmic mean temperature difference)

$$\Delta T_m = \frac{\Delta T_1 - \Delta T_2}{\ln \left( \frac{\Delta T_1}{\Delta T_2} \right)}$$

Where,

$$\Delta T_1 = T_{h1} - T_{c2}$$

$$\Delta T_2 = T_{h2} - T_{c1}$$

#### 3.6. Nusselt Number for cold water flowing through the annular space.

$$Nu_o = 0.023 (Re_o)^{0.8} (Pr)^{0.3}$$

$$Re_o = \frac{U_o D_h \rho}{\mu}$$

Where,  $D_h = D_i - d_o$

Continuity equation

$$m_c = A_o U_o \rho$$

#### 3.7. Cold water heat transfer coefficient flowing through the annular space between two tubes.

$$Nu_o = \frac{h_o D_h}{K}$$

$$h_o = \frac{Nu_o K}{D_h}$$

#### 3.8. Hot water heat transfer coefficient flowing through the inner tube.

$$\frac{1}{U} = \frac{1}{h_o} + \frac{1}{h_i}$$

Where,  $h_i = \frac{1}{\left(\frac{1}{U} - \frac{1}{h_o}\right)}$

**3.9. Hot water Nusselt Number of flowing through the inner tube- experimental.**

$$Nu_i = \frac{h_i d_i}{K}$$

**3.10. Theoretical Nusselt Number by Dittus-Boelter equation of hot nanofluid flowing through the inner tube**

$$Nu_i = 0.023(Re_i)^{0.8} (Pr)^{0.3}$$

**3.11. Friction Factor (Experimental)**

(i)  $\Delta P = h \rho g$

(ii)  $\Delta P = \frac{f L \rho U_i^2}{2 d_i}$

Where,  $f = \frac{2 g d_i h}{L U_i^2}$

**3.12. Friction Factor (Theoretical)**

$$f = 0.0055 \left( 1 + \left( 50 + \left( \frac{10^6}{Re_i} \right)^{0.33} \right) \right)$$

**3.13. Performance evaluation criteria**

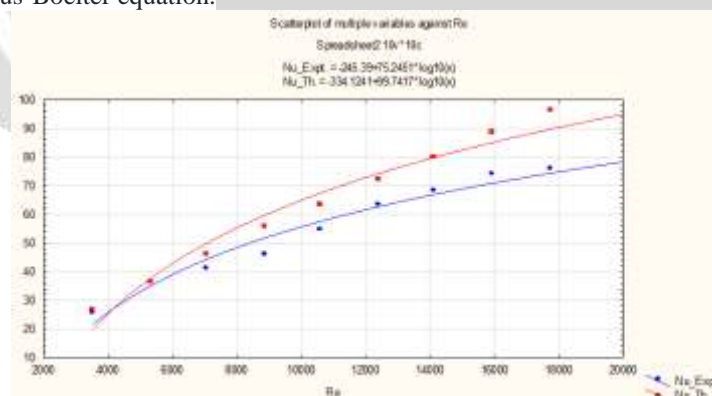
$$PEC = \eta = \left( \frac{Nu \frac{P_i}{f_s}}{Nu \frac{P_i}{f_p}} \right)$$

**4. Results and discussions**

By conducting initial experiments using simple tube in tube heat exchanger, it was possible to discover the precision with which the Nusselt number and friction factor could be experimentally calculated using the current experimental setup. The outcomes are contrasted with established empirical relationships and earlier studies on turbulent flow. The goal was to evaluate the apparatus's dependability.

**4.1. Theoretical and experimental heat transfer for plain smooth tube**

The correlation between Reynolds number and Nusselt number is represented in Figure-9. The graph reveals the correlation between Nusselt number and Reynolds number. With a maximum 20% difference, the numbers closely match the Dittus-Boelter equation.



**Figure-9:** Nusselt number v/s. Reynolds number for plain smooth tube

**4.2. Theoretical and experimental and friction factor for plain smooth Tube**

The association among Reynolds number and friction factors for turbulent flow in a plain smooth tube is showed in figure-10. The attained findings are relatively nearby to theoretic values. This exhibits that the experimental test rig is authenticated and allowing for the conduct of more further experiments.



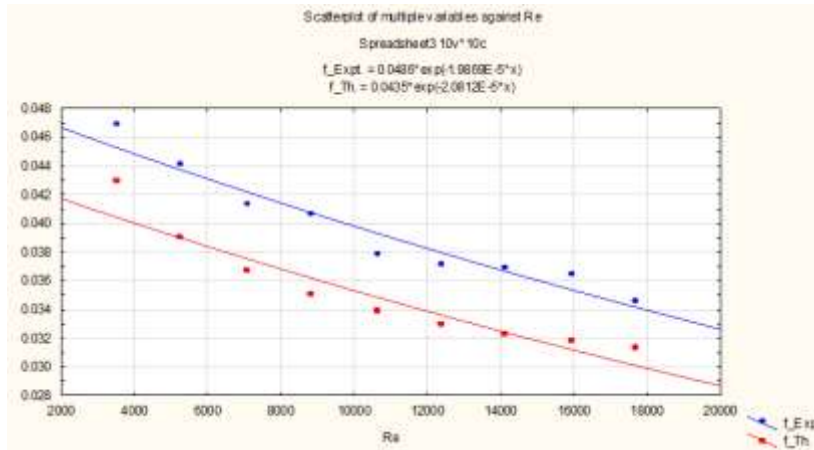


Figure-10: Friction factor v/s. Reynolds number for smooth plain tube

4.3. "Smooth Plain Tube" Vs. "Tubes with various twisted tape inserts"

The correlation between Nusselt number and Reynolds number for smooth plain tubes and tubes with different inserts is described in Figure-11. According to the following graph, Nusselt number is a function of Reynolds number. When Reynolds numbers increase, the Nusselt number also rises. Therefore, a higher Reynolds number results in a greater rate of convective heat transfer.

Furthermore, it can be comprehended that for a given Reynolds number, twisted tapes with a smaller twist ratio provide the largest Nusselt numbers. Twisted tape inserts with a lower twist ratio have a improved rate of heat conduction.

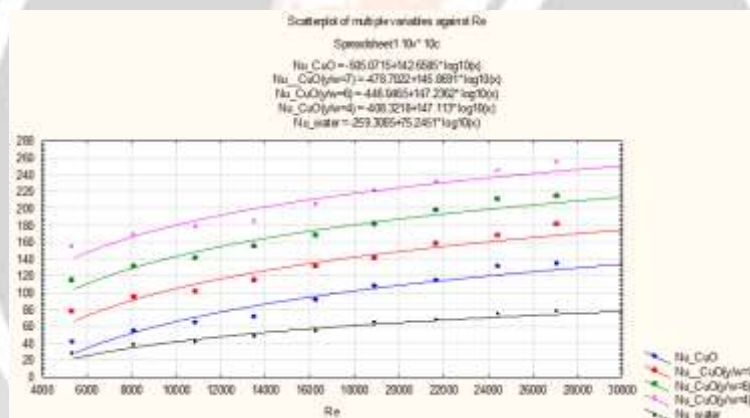


Figure-11: Nusselt Number v/s. Reynolds number graph for (Y = 7, 6, 4), CuO, and water

The correlation between Reynolds number and friction factor for smooth plain tubes and tubes with altered inserts is shown in Figure-12. The graph specifies that for a plain tube, friction is minimal. For a given Reynolds number, the friction factor keeps growing as the twist ratio shrinkages.

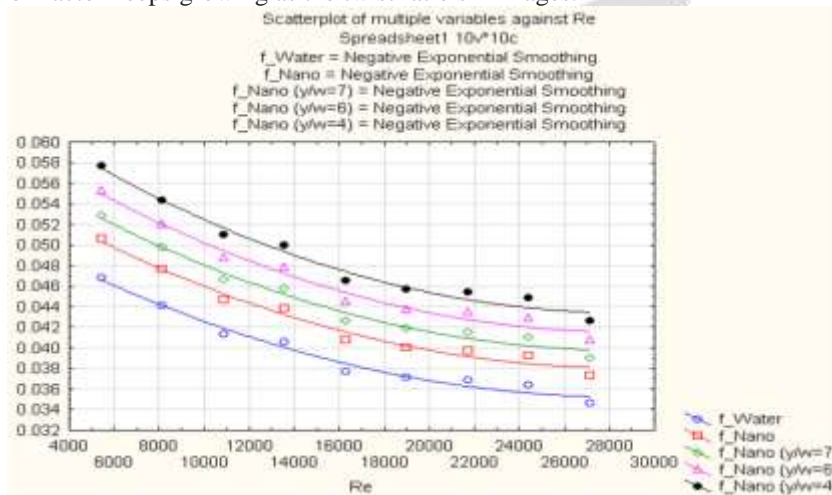


Figure-12: Friction factor v/s. Reynolds number graph for (Y = 7, 6, 4), CuO, and water

## 5. Conclusion

In the present work, CuO-water nanofluid with different twist ratios and a circular tube equipped with full-length square jagged twisted tape inserts have been studied experimentally for Nusselt number and friction factor. The outcomes are distinguished with those of a plain tube filled with base fluid. CuO/water nanofluid with square jagged twisted tape insert with twist ratio=4 can produce a maximum Nusselt number of 72%, which is higher than that of the base fluid. The results showed a considerable improvement in heat transfer, and the performance of the proposed nanocomposite for improving the thermal performance of heat exchangers in the chemical and petroleum industries was superior with smaller twist ratios.

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