

# VARIATION OF MINIMUM FILM THICKNESS WITH RESPECT TO SHAFT SPEED FOR NEWTONIAN AND NON NEWTONIAN FLUIDS IN JOURNAL BEARING

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## ABSTRACT

Journal bearing are designed to carry radial loads and are made cylindrical and ring shaped. The journal bearing has several advantages over other types of bearing, providing it has a constant supply of clean high-grade motor oil. Journal bearings with their inherent advantages are also used in other high-load, high-velocity applications, such as machines and turbines.

In this paper, I have studied about the steady state analysis for Lubrication in Journal Bearing. To describe the lubrication rheology the effect of Non-Newtonian fluid behavior has been studied by assuming Ree-Eyring Model. The assumption of isothermal condition has been considered for the sake of simplicity.

**Keyword:** - Journal Bearing, Newtonian Fluid, Non-Newtonian Fluid

## 1. INTRODUCTION

One of the most important design problems is to support a load in the presence of relative motion. According to the motion the load can be radial and axial or both radial and axial depending upon the motion i.e. translator or rotary. The parts used for supporting such load are called bearing. Hence the bearing may be defined as a machine member whose function is to support and retain a moving member. Depending upon the type of friction, bearing are classified into two main group sliding contact bearing and rolling contact bearing. Sliding contact bearings are also called plain bearings, journal bearing or sleeve bearing.

### 1.1 JOURNAL BEARING

The journal bearing has several advantages over other types of bearing, providing it has a constant supply of clean high-grade motor oil. First, it handles high loads and velocities because metal to metal contact is minimal due to the oil film. Second, the journal bearing is remarkably durable and long lasting. Finally, because of the damping effects of the oil film, journal bearings help make engines quiet and smooth running. Journal bearings with their inherent advantages are also used in other high-load, high-velocity applications, such as machines and turbines.

## 2. GOVERNING EQUATION

The basic equation for journal bearing which governs the generation of pressure in lubricating films is known as Reynolds equation and it forms the foundation of hydrodynamic lubrication analysis. It was derived for a Newtonian fluid by neglecting the effects due to curvature of fluid film. This assumption is well justified as the effective radius of bearing components is generally very large compared with the film thickness. This enables the analysis to consider an equivalent curved surface near a plane.

The derivation of Reynolds equation involves the application of the basic equation of motion and continuity to the lubricant.

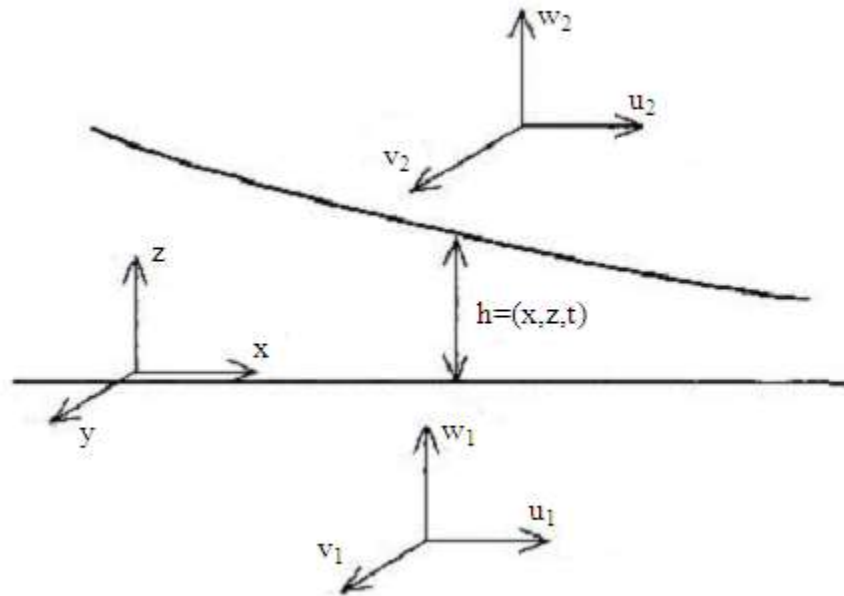
### Assumptions

1. Thin film geometry

2. The fluid is Newtonian and the coefficient of viscosity is constant.
3. Compressibility of the fluid is negligible.
4. There is no slip between the fluid and the solid surface.
5. Fluid pressure does not change across the film thickness.
6. The rate of change of the velocity  $u$  and  $w$  in the  $x$  direction and  $z$  direction is negligible compared with the rate of change in the  $y$  direction.

The basic theory of Reynolds equation can be understood by using the above assumption and with the help on the axes of rectangular coordinates  $x$ ,  $y$ , and  $z$  are taken as shown in the figure. The  $x$  and  $y$  axes are on the lower surface and the  $z$  axis is perpendicular to it. The velocity of the fluid in the directions  $x$ ,  $y$ , and  $z$  are denoted by  $u$ ,  $v$  and  $w$ , respectively, and the velocity of the lower surface is similarly described by  $u_1$ ,  $v_1$ , and  $w_1$  and that of the upper surface by  $u_2$ ,  $v_2$ , and  $w_2$ . In many practical cases, the lower surface and the upper surface perform a straight translational motion relative to each other. In this case, if the  $x$  axis is in the translational direction, then we have  $w_1 = w_2 = 0$  and so the equations can be simplified.

Let the gap between the two surfaces, or the thickness of the liquid film, be denoted by  $h(x, z, t)$ , with  $t$  being time. Let the coefficient of viscosity of the fluid be  $\eta$ .



**Fig. 2 Fluid film between two solid surfaces**

The derivation of Reynolds equation involves the application of the basic equation of motion and continuity to the lubricant. The full equations of motion for a Newtonian fluid in Cartesian coordinates are:

$$\rho \frac{du}{dt} = \rho X - \frac{\partial p}{\partial x} + \frac{2}{3} \frac{\partial}{\partial x} \eta \left( \frac{\partial u}{\partial x} - \frac{\partial w}{\partial z} \right) + \frac{2}{3} \frac{\partial}{\partial x} \eta \left( \frac{\partial u}{\partial x} - \frac{\partial v}{\partial y} \right) + \frac{\partial}{\partial y} \eta \left( \frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \right) + \frac{\partial}{\partial z} \eta \left( \frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right) \tag{2.1a}$$

$$\rho \frac{dv}{dt} = \rho Y - \frac{\partial p}{\partial y} + \frac{2}{3} \frac{\partial}{\partial y} \eta \left( \frac{\partial v}{\partial y} - \frac{\partial u}{\partial x} \right) + \frac{2}{3} \frac{\partial}{\partial x} \eta \left( \frac{\partial v}{\partial y} - \frac{\partial w}{\partial z} \right) + \frac{\partial}{\partial z} \eta \left( \frac{\partial v}{\partial z} - \frac{\partial w}{\partial y} \right) + \frac{\partial}{\partial x} \eta \left( \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) \tag{2.1b}$$

$$\rho \frac{dw}{dt} = \rho Z - \frac{\partial p}{\partial z} + \frac{2}{3} \frac{\partial}{\partial z} \eta \left( \frac{\partial w}{\partial z} - \frac{\partial u}{\partial x} \right) + \frac{2}{3} \frac{\partial}{\partial z} \eta \left( \frac{\partial w}{\partial z} - \frac{\partial v}{\partial y} \right) + \frac{\partial}{\partial x} \eta \left( \frac{\partial w}{\partial x} - \frac{\partial z}{\partial z} \right) + \frac{\partial}{\partial y} \eta \left( \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \right) \tag{2.1c}$$

The terms on the left hand side represent inertia effects and on the right hand side are the body force, pressure and viscous terms in that order. The inertia and body forces are negligible as compared to the viscous and inertia forces.

The equation of continuity representing conservation of mass is:

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} + \frac{\partial \rho w}{\partial z} = 0 \tag{2.2}$$

Using the above equations 2.1a, 2.1b, 2.1c and 2.2, general Reynolds equation is:

$$0 = \frac{\partial}{\partial x} \left( -\frac{\rho h^3}{12\eta} \frac{\partial p}{\partial x} \right) + \frac{\partial}{\partial y} \left( -\frac{\rho h^3}{12\eta} \frac{\partial p}{\partial y} \right) + \frac{\partial}{\partial x} \left( \frac{\rho h(u_a + u_b)}{2} \right) + \frac{\partial}{\partial y} \left( \frac{\rho h(v_a + v_b)}{2} \right) + \rho(w_a - w_b) - \rho u_a \frac{\partial h}{\partial x} - \rho v_a \frac{\partial h}{\partial y} + h \frac{\partial \rho}{\partial t} \tag{2.3}$$

For only tangential motion, where

$$w_a = u_a \frac{\partial h}{\partial x} + v_a \frac{\partial h}{\partial y} \quad \text{and}$$

$$w_b = 0,$$

The Reynolds equation given in equation (2.3) becomes

$$\frac{\partial}{\partial x} \left( \frac{\rho h^3}{\eta} \frac{\partial p}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{\rho h^3}{\eta} \frac{\partial p}{\partial y} \right) = 12\hat{u} \frac{\partial(\rho h)}{\partial x} + 12\hat{v} \frac{\partial(\rho h)}{\partial y} \tag{2.4}$$

$$\hat{u} = \frac{u_a + u_b}{2} = \text{constant} \qquad \hat{v} = \frac{v_a + v_b}{2} = \text{constant}$$

Equation (2.4) is applicable for elastohydrodynamic lubrication.

If there is axisymmetry, so that the model can be treated as a one-dimensional problem; then the Reynolds equation for an incompressible lubricant can be written as:

$$\frac{\partial}{\partial x} \left( \frac{h^3}{12\eta} \frac{\partial p}{\partial x} \right) = \frac{u}{2} \frac{\partial h}{\partial x} + \frac{\partial h}{\partial t} \quad (2.5)$$

In the equation  $p$  represents the film pressure,  $\eta$  denotes the lubricant viscosity,  $u$  is the sliding velocity of the lower surface,  $h$  is the film thickness depending upon the coordinate.

### 3. SOLUTION PROCEDURE

The steps involved in the overall solution scheme are given below:

1. The pressure distribution [P], minimum film thickness  $H_0$  and outlet boundary co-ordinate  $X_0$  were initialized to some reference values. Take  $X_{in}=0$  and  $X_0=1$ .
2. Evaluated the fluid film thickness,  $H$ , at every node by using film thickness equation.
3. The residual vector [f] was calculated at each node.
4. The residual vector  $\Delta W$  was calculated from the discretized load equilibrium equation.
5. The residual vectors calculated in the steps 3 and 4 were assembled in a single vector [F] to facilitate execution of Newton-Raphson scheme.
6. This was followed by computation of Jacobian coefficients.
7. The corrections to the system variables were computed by inverting the Jacobian matrix using Gauss elimination.
8. The corrections, calculated in step 7, were added to the corresponding system variables to get the new values of the pressure distribution [P] and minimum film thickness  $H_0$ .
9. The outlet boundary co-ordinate  $X_0$  was corrected by using an appropriate scheme.
10. The termination of the iterative loops required the fulfillment of the predefined convergence criteria to arrive at an accurate solution. In order to check the convergence of the pressure distribution, the sum of the nodal pressures corresponding to the current iteration (say  $n^{th}$ ) was calculated. If the fractional difference between this value and that corresponding to the previous iteration was less than the prescribed tolerance TOL, the pressure distribution was assumed to have converged. Thus,

$$\frac{\left| \left[ \sum_{i=1}^N P_i \right]_n - \left[ \sum_{i=1}^N P_i \right]_{n-1} \right|}{\left| \left[ \sum_{i=1}^N P_i \right]_{n-1} \right|} \leq TOL$$

11. The minimum film thickness was assumed to converge if the fractional change in its value became less than the prescribed tolerance in successive iterations

$$\frac{\left| \left[ H_o \right]_n - \left[ H_o \right]_{n-1} \right|}{\left| \left[ H_o \right]_{n-1} \right|} \leq TOL$$

The value of TOL adopted in the analysis was  $1 \times 10^{-4}$  as it has been found that a lower value does not contribute to improve the accuracy of the solution. The iterative loop terminates and the current values were considered as the final solution only if all the relevant convergence criteria were satisfied simultaneously.

12. If any one or more of the relevant criteria were not satisfied, the next iteration began and the control was shifted back to the step 2.
13. Finally the values of pressure distribution, minimum film thickness, friction coefficient and attitude angle calculated using suitable formulae.

#### 4. RESULTS AND DISCUSSION

The results have been obtained for effect of shaft speed on the minimum film thickness for Newtonian and non Newtonian fluids. The value of radial load i.e.  $W=150000\text{N/m}$  and radial clearance i.e.  $C=0.005\mu\text{m}$  have been taken constant for both Newtonian and non Newtonian fluids.

Figure 4.1 shows the variation of minimum film thickness ( $H_{\min}$ ) with respect to speed ( $u$ ) for Newtonian and non Newtonian fluids. The solid line shows the results for Newtonian fluid, dotted line shows the results for first type of non-Newtonian fluid and dashed line shows the results for second type of non-Newtonian fluid. It can be observed from figure that the value of increase in minimum film thickness is almost similar for Newtonian fluid and for first type of non-Newtonian fluid, and greater than the second type non-Newtonian fluid

A quantitative comparison value of minimum film thickness with speed is given in the table 4.1. It can be observed from table that for Newtonian fluid there is an increase of 116% in the value of minimum film thickness when the speed is increased from 1m/sec to 3m/sec i.e. by increasing the speed by 200%, similarly there is an increase of 17% in the value of minimum film thickness when the speed is increased from 3m/sec to 6m/sec i.e. by increasing the speed by 100% and there is an increase of 6% in the value of minimum film thickness when speed is increased from 6m/sec to 10m/sec i.e. by increasing the speed by 66%.

For first type of non Newtonian fluid with similar increase in the value of speed i.e. 200%, 100% and 66% there is an increase of 113%, 14% and 3.5% respectively in the value of minimum film thickness, similarly for second type non Newtonian fluid with same increase in the value of speed there is an increase of 42.66%, 4.7% and 1.0% respectively in the value of minimum film thickness.

**Table4.1 Effect of change in speed on minimum film thickness**

Fluid	Percentage change in shaft speed	Percentage Change in minimum film thickness
Newtonian Fluid	Increase by 200%	Increase by 116%
	Increase by 100%	Increase by 17%
	Increase by 66%	Increase by 6%

Non Newtonian Fluid 1	Increase by 200%	Increase by 113 %
	Increase by 100%	Increase by 14 %
	Increase by 66%	Increase by 3.5 %
Non Newtonian Fluid 2	Increase by 200%	Increase by 42.66 %
	Increase by 100%	Increase by 4.7 %
	Increase by 66%	Increase by 1.0 %

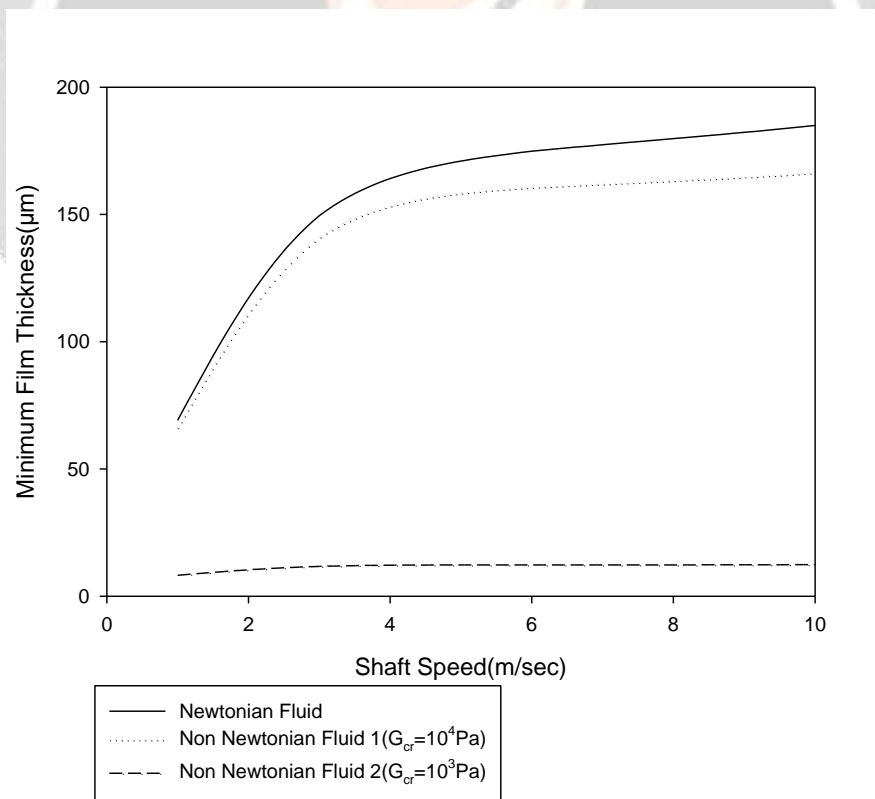


Fig 4.1 Variation of minimum film thickness with speed(C=0.005 µm, W=150000N/m)



## 5. REFERENCES

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